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EXAM	MINER INTERVIEW SUMMARY RECO	RD
All participants (applicant, applicant's representative, P	TO personnel):	
1) Eric W. Guttay/George	W. Aller (3) Everett	White (PTO)
11) Eric W. Guttag/George 12) Pat J. Corriga	(4) Johnnie	R. Brown
Date of interview May 28, 1992		
Type: 🔲 Telephonic 🔑 Personal (copy is given to	applicant applicant's representative	
Exhibit shown or demonstration conducted: 🚨 Yes	□ No. If was brief description.	
exhibit shown or demonstration conducted.   Tes	No. 11 yes, brief description:	
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Agreement 🙎 was reached with respect to some or al	I of the claims in question.	ned
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Claims discussed: <u>All the Klaims o</u>	t record	
Identification of prior art discussed: $\frac{a}{-a}$	prior ant of record	
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Description of the general nature of what was agreed to	if an agreement was reached, or any other com	nments: The Attorney proposed to submi
		tion. It is the Examiner's opinion
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hot this new claim will require	further consideration and the	wither scapech. Mr. Corrigan expla
•		ioned why US Patent No 5,043,43
ind European Patent No. 383, 404 m		
NICTS) 9KT ON THE PART OF THE EXAMPLE A fuller description, if necessary, and a copy of the	mer. amendments, if available, which the examiner	agreed would render the claims allowable must be
ttached. Also, where no copy of the amendments whic	th would render the claims allowable is available	e, a summary thereof must be attached.)
Inless the paragraphs below have been checked to inc IOT WAIVED AND MUST INCLUDE THE SUBSTA ast Office action has already been filed, then applicant	NCE OF THE INTERVIEW (e.g., items 1-7	on the reverse side of this form). If a response to the
(It is not necessary for applicant to provide a sepa	arate record of the substance of the interview.	
		te response to each of the objections, rejections and labele, this completed form is considered to fulfill the
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	Evaminer	'e Signature

## PROPOSED NEW CLAIM 62 FOR CASE 4233

- 62. A continuous process for preparing highly esterified polyol fatty acid polyester by interesterifying polyol containing more than about four esterifiable hydroxy groups and fatty acid ester of easily removable alcohol in a heterogeneous reaction mixture wherein said easily removable alcohol is removed, said process comprising an improvement selected from the group consisting of:
  - the initial stage of the reaction is carried out in a continuous manner under conditions of backmixing to maintain a level of lower partial fatty acid esters of said polyol in an emulsifying amount;
  - (2) at least the final stage of the reaction is carried out in a continuous manner under conditions approaching plug-flow conditions after the degree of esterification of said polyol is at least about 50%; and
  - (3) a combination of improvements (1) and (2).

Support for new Claim 62: Claim 1, Claim 34 and page 23, lines 19-21.

(4233R3)

## Interview for Case 4233

- I. Applicants' Claimed Improved, Preferably Continuous, Processes for Preparing Highly Esterified Polyol Polyesters
  - A. Ten separate process improvements, plus combinations of these improvements. See Claim 1.
  - B. Claimed process improvements offer a number of significant advantages, including:
    - 1. increased reaction speed and efficiency;
    - 2. reduced/minimized formation of undesired/unwanted by-products;
    - 3. reduced/minimized need to remove excess reactants/catalyst
    - greater conversion to desired highly esterified polyol polyester end products
    - 5. easier clean-up of desired end products
    - reduced/minimized capacity/energy requirements for equipment used and increased process flexibility.
  - C. Handout Explaining Reaction Chemistry of Claimed Process
    Improvements (Pat Corrigan)

- 1. In general.
- 2. As it relates specifically to "backmixing" in initial stage and "plug-flow" in final stage(s).

## II. Proposed New Claim 62

- A. Recites continuous process involving:
  - "backmixing" conditions in initial stage to maintain emulsifying amount of partial esters;
  - "plug-flow" conditions in final stage(s) after degree of esterification reaches 50%; and
  - 3. combination of "back mixing" and "plug-flow" conditions.
- B. If allowable, Claims 14-16, 27-51 and 54-58 would be amended to depend therefrom.

III. The Rejection of Claims 1, 14-16, 27-51 and 54-58 under 35 USC 103 over Volpenhein, in View of Osipow et al, as it Relates to "Backmixing" and "Plug-Flow."

## A. "Backmixing"

- Requires: (a) continual recycling of portion of reactant mixture; or (b) carrying out reaction in agitated vessel(s) with continual addition of reactants and removal of product.
   See paragraph bridging pages 19-20 of Case 4233.
- Volpenhein and Osipow et al nowhere teach reaction conditions that inherently involve "backmixing."

## B. "Plug-FLow"

- Requires (a) feeding output of initial stage into at least 2 CSTRs; or (b) use of continuous reactor, e.g., tubular reactor.
   See page 21, lines 27-33 of Case 4233.
- Volpenhein and Osipow et al nowhere teach reaction conditions that inherently involve "plug-flow."

Sucrose Polyester

**Reaction Chemistry** 

## The sucrose polyester reaction has four main raw materials:

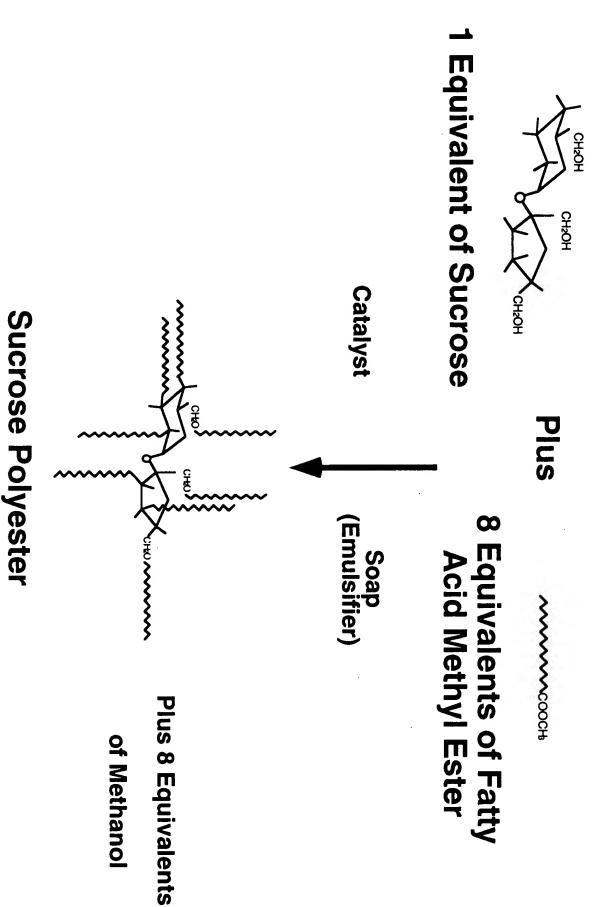
Sucrose

**Fatty Acid Methyl Esters** 

Soap

Catalyst

# **Basic Sucrose Polyester Reaction**



# Sucrose Polyester Reaction Involves 2 Steps:

Solubilize the solid sucrose into the liquid methyl esters

2. Esterify the methyl esters with the sucrose

# Materials that help solubilize the sucrose:

~~~~~COO-K+

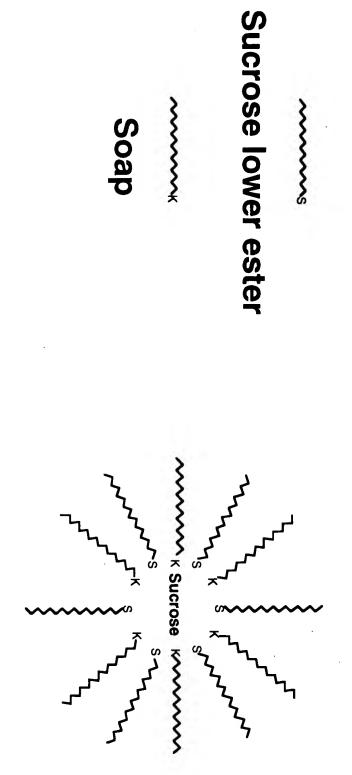
(Soap)

CH2OH CH2OH

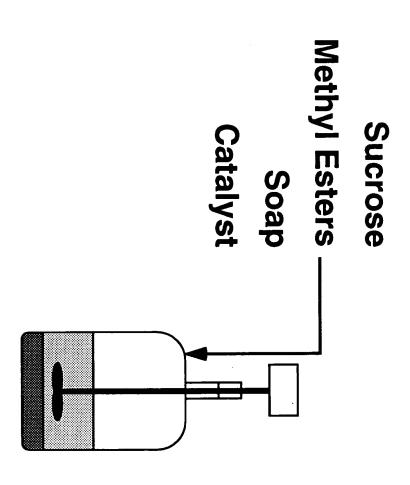
**Lower Esters of Sucrose** 

**Both** are required

## **Inverted Micelles**



## **Batch Reaction**

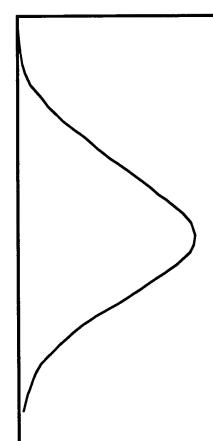


First part of the reaction:

Sucrose + Methyl Ester -----> Sucrose Lower Esters

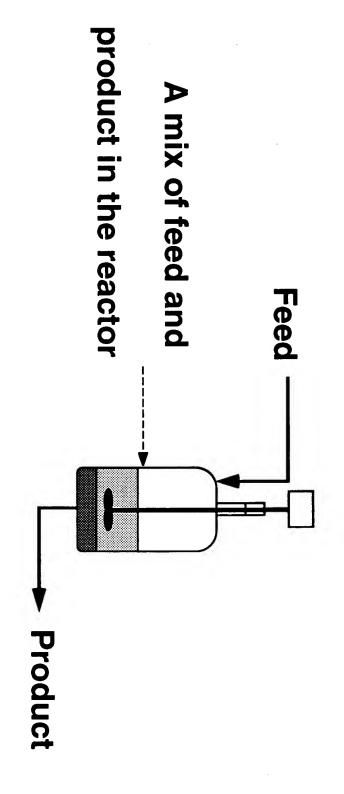
# **Sucrose Lower Esters versus Time**

Amount of Sucrose
Lower Esters



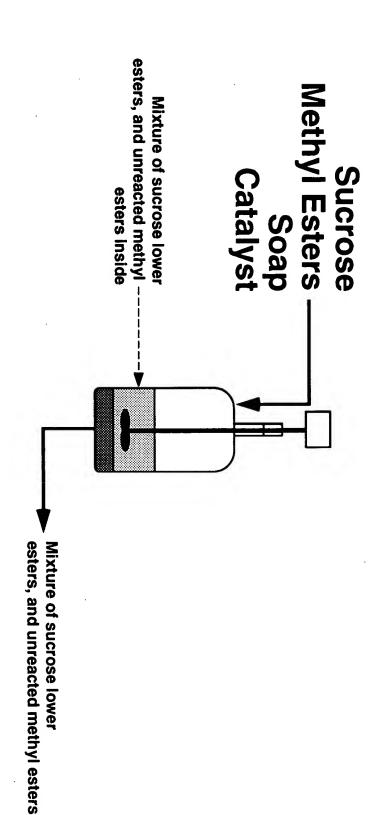
Reaction Time ---->

# **A Continuous Backmixed Reactor**



# A Continuous Backmixed Reactor

## to Make Sucrose Lower Esters



the basic reaction for the formation of sucrose polyester Once the sucrose has reacted to sucrose lower ester, S

sucrose ester + methyl ester ---V sucrose polyester + methanol

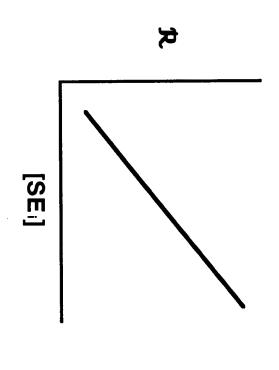
Reaction rate = 
$$\Re = \frac{k[SE_i][ME]}{[MeOH]}$$

[MeOH] ----> also constant with respect to [SE<sub>i</sub>]. There is an excess of methyl esters in the reaction: Methanol is continuously removed by vacuum: [ME] -----> constant (with respect to [SE<sub>i</sub>])

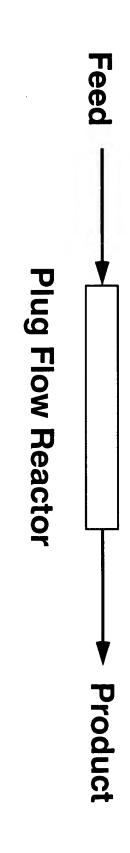
Then: 2 = K[SEi] where K = k[ME][MeOH]

R is proportional to [SE<sub>i</sub>]

R is proportional to [SE<sub>i</sub>]



## **Plug Flow Reactor**



a plug flow reactor 

is equivalent to

2 or more backmixed reactors

## **Final Conclusions:**

The optimum method to run this reaction on a practical scale is:

1. Run the first part of the reaction in a continuous, backmixed mode;

2. Run the subsequent part of the reaction in a plug flow mode.